



Final campaign report

Development of a safe and scalable process for the synthesis of pyrrolo[2,1-f][1,2,4]triazin-4-amine

Submitted to

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TCG GreenChem and Life sciences Pvt. Limited – Contract development and manufacturing organization (CDMO)

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Major Scope of the work:

- Feasibility study of the proposed route
- Analytical method development for in-process control and release of the intermediates as well as final compound
- Optimization of the reaction in terms of yield, quality, time and safety
- Comprehensive safety studies of the optimized protocol
- Impurity profiling
- Synthesis of 1.0 Kg of the target pyrrolo[2,1-f][1,2,4]triazin-4-amine
- Preparation of lab development report and submit





Overview:

Pyrrolo[2,1-f][1,2,4]triazin-4-amine is a key starting material of Remdesivir which is one of the front line drug for the treatment of COVID-19. Structure of the Target compound is shown below.



Summary of work done and major accomplishments

- Various conditions were screened for all the steps and based on the study, a safe and scalable protocol has been established for the synthesis of target compound in Kg scale
- Extensive safety studies have been performed using RC1 and DSC to identify the safe protocol for scale up
- Many process impurities have been identified, isolated, synthesized and characterized
- Efficient purification protocol has been established to purge most of the process impurities
- Eventually final target compound has been synthesized on 1Kg scale with purity >99.9% with assay 98.4%











TCG Lifesciences CHEMBIOTEK

TCG LIFESCIENCES PRIVATE LIMITED						
CERTIFICATE OF ANALYSIS						
Product Name :	PYRROLO[2,1-f][1,2,4]	TRIAZIN-4-AMINE (R	MD-B-II)			
Product Code :	Product Code : RMD-B-II Date of Analysis : 28/09/2020					
Batch No. :	CR592-15274-96-P	Date of Mfg. :	SEP-2020			
Sample Quantity : 1050.0 g Retest Period : FEB-2021						
STP No. :	NA	•	·			

S. No.	Test	Acceptance criteria	Results
1	Description	Report result	Brown solid
	Identification by		
	IR spectrophotometry	The characterization of sample by infrared absorption spectrum exhibit the pattern of functional groups present in structure of the molecule	Complies
2	NMR (1H,13C)	The characterization of sample by NMR spectrum should confirm to the structural identity of the molecule	Complies
	Mass spectrophotometry (GCMS)	The characterization of sample by mass spectrum should obtain same molecular weight obtained by empirical formula	Complies
3	Water content by KF (% w/w)	Report result	0.20
4	Loss on drying (% w/w)	Report result	0.35
5	Chromatographic purity by HPLC (% area)	Report result	99.9
6	Assay by titration (% w/w)	Report result	98.4

Remarks: This material Complies/Does not comply to the above specification.

Prepared by	Reviewed by	Approved by
Sign: Parthe Barn	Sign: A. Nanofinish	Sign: Sebajnet Shevrike
Date: 01/10/2020	Date: 01/10/2020	Date: 01/10/2020
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Final optimized synthetic scheme

Final optimized synthetic scheme is shown below.







Step-1

Actual batch size and quantity:

S. No.	Reagent		Unit	Qty	Mol Wt	Mole	Mole ratio/ wt times vol	Source
1	Pyrrole		g	1000	67.09	14.90	1	Commercial
2	Phosphorus oxyc	hloride	mL	1544	153.33	16.56	1.11	Commercial
3	Hydroxylamine hydrochloride		g	1139	69.49	16.38	1.09	Commercial
4	Acetic anhydride		mL	1548	102.08	16.48	1.10	Commercial
5	Pyridine		mL	6000	79.10	74.18	4.97	Commercial
6	Due e este vue te u	Lot-1	T	3000			3 vol	
0	Process water	Lot-2	mL	10000	-		10 vol	
7	N,N- Dimethylformamide (anhydrous)		mL	10000	-		10 vol	Commercial
		Lot-1		10000	-		10 vol	
8	Methyl <i>tert</i> -butyl ether (MTBE)	Lot-2	mL	10000			10 vol	Commercial
		Lot-3		10000			10 vol	
9	2 N Hydrochloric	acid	mL	10000	-		10 vol	Commercial
10	Aq. Sodium bicarbonate solution (10%)	Lot-1		10000			10 vol	Communici
		Lot-2	mL	10000	-		10 vol	Commercial
11	Anhydrous Sodiu sulfate	m	g	1000	-		1 w/w	Commercial

a) Process:

S.No.	Procedure	Qty.	Remarks
1.	Check the cleanliness of the reaction vessel (20 L		
	3-necked flask) fitted with an internal temperature		
	probe, overhead stirrer, and addition flask and		
	nitrogen line.		





S.No.	Procedure	Qty.	Remarks
2.	Charge anhydrous DMF (10000 mL) into the reaction flask.	10000 mL	
3.	Cool the reaction vessel under N_2 atmosphere so that internal temperature of the flask remains between 0-5 °C		
4.	Stir the contents of the vessel at 0-5 °C.		
5.	Charge phosphorus oxychloride (1544 mL) slowly into the reaction vessel maintaining the internal temperature of the vessel at 0-5°C	1544 mL	Time : ~ 3.0 h
6.	Raise the reaction mixture to 15-20°C.		
7.	Stir the mixture at 15-20 °C for another 30 min.		
8.	Cool the mixture again to 0-5 °C.		
9.	Charge pyrrole (1000 g) slowly into the cooled reaction mixture maintaining the internal temperature of the vessel below 15 °C.	1000 g	Time : 1.5 h
10.	Stir the mixture at 15-20 °C for another 1 h.		
11.	Cool the light brown mixture to 0-5 °C.		
12.	Charge process water lot-1 (3000 mL) slowly (2- 3 h) into the reaction mixture maintaining the internal temperature of the mixture below 15 °C.	3000 mL	
13.	Stir the mixture at 15 °C for 5 min.		
14.	Charge solid hydroxylamine hydrochloride (1139.2 g) into the mixture while maintaining the internal temperature below 15 °C.	1139.2 g	
15.	Charge acetic anhydride (1548 mL) into the mixture while maintaining the internal temperature below 15 °C.	1548 mL	
16.	Charge pyridine (6000 mL) into the mixture while maintaining the internal temperature below 15 °C.	6000 mL	
17.	Heat the reaction mixture to 90 °C and stir the mixture at this temperature for 16 h.		
18.	Send the sample of the reaction mixture for HPLC analysis to check the complete consumption of Aldehyde (IPC-1). Sample preparation: Take sample directly from reaction mass and submit as such		IPC-1 (Aldehyde NMT 2%) Result: Below detection limit
19.	Cool the reaction mass to 25-30°C.		
20.	Charge chilled (10-15°C) process water lot-2 (10000 mL) into the reaction mass and stir the mass for 10 min.	10000 mL	
21.	Charge MTBE Lot-1 (10000 mL) into the mixture and stir the mixture for 10 min	10000 mL	
22.	Stop the stirring and allow the reaction mixture for layer separation.		





S.No.	Procedure	Qty.	Remarks
	Separate the organic and aqueous layer (with the		
23.	help of separatory funnel) into two separate clean		
	containers.		
	Charge back the aqueous layer into the reaction		
24.	vessel again and charge MTBE Lot-2 (10000	10000 mL	
	mL) into it.		
25	Stir the mixture for 10 min. Stop the stirring and		
	allow it for layer separation.		
•	Separate the organic and aqueous layer (with the		
26.	help of separatory funnel) into two separate		
	containers.		
27	Charge back the aqueous layer into the reaction	10000 1	
27.	vessel again and charge NIIBE Lot-3 (10000	10000 mL	
	IIL) IIIO II.		
28.	still the initiale for 10 min. Stop the stiffing and		
	Separate the organic and aqueous layer (with the		
29	help of separatory funnel) into two separate		
27.	containers		
	Charge the combined organic layers into the		
30.	reaction vessel.		
21	Charge 2N Hydrochloric acid into the reaction	10000 1	
31.	vessel and stir the contents for 10 min.	10000 mL	
32.	Stop the stirring and allow it for layer separation.		
33.	Separate the aqueous layer.		
	Charge 10% aqueous sodium bicarbonate		
34.	solution (10000 mL) into the reaction vessel and	10000 mL	
	stir the contents for 10 min.		
35.	Stop the stirring and allow it for layer separation.		
36.	Separate the aqueous and organic layer.		
	Charge 10% aqueous sodium bicarbonate		
37.	solution (10000 mL) into the reaction vessel and	10000 mL	
	stir the contents for 10 min.		
38.	Stop the stirring and allow it for layer separation.		
39.	Separate the aqueous layer and organic layer into		
	two separate containers.		
40.	layer allows it for 15 min for drying.	1000 g	
	Charge the dried organic layer into the reaction		The vield of crude dark
41.	vessel and distil out the organic layer under		brown liquid = 1380 g
	medium reduced pressure at 40-50 °C.		
			First fraction (~10-15%)
	Purify the crude by fractional distillation. Desired		contains mostly DMF
42.	product starts to distill off at 100-140 °C under		and volatiles. Second
	ĥigh vacuum pressure (2-4 mm Hg).		iraction onwards desired
			collect





S.No.	Procedure	Qty.	Remarks
43.	Send the distillate for checking purity by HPLC.		Purity by HPLC NLT 95% Assay by HPLC : Report result Assay of DMF by GC: Report result
44.	Yield range (1-1.2 w/w)		Yield is based on assay by HPLC

In process controls data:

Batch Id	IPC-1 (Limit: NMT 2 %)	Crude Purity by HPLC
CR592-15288-25	IPC-01.pdf	Crude-Purity by HPLC.pdf
	Aldehyde (15.8 min) Balaw datastian limit	
	Batch Id CR592-15288-25	Batch IdIPC-1 (Limit: NMT 2 %)CR592-15288-25Image: Decoular of the second secon

Purification of Crude 2-cyanopyrrole to pure fraction:

Crude 2-cyanopyrrole was taken in a 2L single neck RBF equipped with distillation condenser and connected to other end with receiver and vacuum line. Set up the vacuum to maximum and slowly start to heat. First fraction collects at 50-70°C and second fraction starts to collect at 95-125°C.

Batch No. CR592-15288-25

Input: 1380.0 g

Yield = (144X 18.2% + 348 X 92.25% + 870 X 89.2%) = 26.0 g + 321.0 g + 776.0 g = 1123.0 g W/w Yield = 1.13 Molar % yield = 81.78%

Fraction-1	Fraction-2	Fraction-3 Residue		Loss
144.0 g	348.0g	870.0g	10.0 g	
Assay 18.2%	Assay: 92.25%	Assay: 89.2%	Assay: 5.0%	8.0g
HPLC area% 94.15%	HPLC area% 99.54%	HPLC area% 99.38%	Not checked	







Step-2:

List of Raw materials

- i) RMD-B-I (1H-pyrrole-2-carbonitrile)
- ii) N,N-Dimethylformamide (DMF)
- iii) 60% Sodium hydride (NaH)
- iv) 12-15% aqueous sodium hypochlorite (NaOCl)
- v) 25% Aqueous ammonia (NH4OH)
- vi) Ammonium chloride (NH₄Cl)
- vii) Anhydrous calcium chloride (CaCl2)
- viii) Methyl tert-butyl ether (MTBE)
- ix) Formamidine acetate
- x) Celite
- xi) Process water
- xii) Sodium chloride

Process Information

Actual batch size and quantity:

S. No.	Reagent	Unit	Qty	Mol Wt	Mole	Mole ratio/ wt times vol	Source
1	1H-pyrrole-2-carbonitrile (Pyrrole-2-carbonitrile)	Kg	0.60	92.04	6.52	1.0 eq	In-house
2	Sodium hydride (60 % dispersion in mineral oil)	Kg	0.29	23.99	7.17	1.1 eq	Commercial
3	Foramidine acetate	kg	2.04	104.11	19.56	3.0 eq	Commercial





S. No.	Rea	Unit	Qty	Mol Wt	Mole	Mole ratio/ wt times vol	Source	
4	Ammonium cl (NH4Cl)	hloride	Kg	2.7	53.49	-	4.5 T	Commercial
5	Ammonia aqu	eous (25%)	L	4.21	-	-	7.02 V	Commercial
6	Sodium hypochlorite solution (Available Chlorine 8-10%)		L	47.4	-	-	79 V	Commercial
-	Methyl <i>tert</i> - butyl ether	Lot-1	Ŧ	36			60 V	
1	(MTBE)	Lot-2		1.2	-	-	2V	Commercial
8	Anhydrous Calcium chloride (CaCl ₂)		Kg	1.2	-	-	2T	Commercial
9	Anhydrous Sodium chloride (NaCl)		Kg	1.80	-	-	3Т	Commercial
10	Anhydrous N,N- Dimethyl	Lot-1	L	6.0			10 V	
10	formamide (DMF)	Lot-2		0.6			1V	Commercial
		Lot-1		12.0				
11	Process water	Lot-2	L	2.4			25 V	
	Water	Lot-3		0.6				

a) Process:

S.No.	Procedure	Qty.	Remarks
	Part-A: Preparation of 3-5% of Monochloroamine		
	in MTBE		
1.	Check the cleanliness of the reactor-1 (fitted with an		
	internal temperature probe, and addition flask and		
	nitrogen line).		
2.	Charge MTBE into the reactor at 25-30 °C	36.0 L	
3.	Charge NH ₄ Cl into the reactor at 25-30 °C	2.7 kg	





4.	Cool the reactor to -8 ± 2 °C (internal temperature)		
5.	Charge Ammonia aqueous (25%) into the reactor keeping the internal temperature -8 ± 2 °C	4.21 L	
6.	Charge pre-cooled (below 5 °C) Sodium hypochlorite solution (chlorine 8-10%) via addition funnel over 50- 80 min into the reactor keeping the internal temperature -8 ± 2 °C	47.4 L	
7.	Stir the contents of the vessel at -8 ± 2 °C for 30 min		
8.	Stop the stirring and settle the reaction mixture for 30- 60 min at -8 ± 2 °C		
9.	Separate the layers		
10.	Wash the organic layer with pre-cooled (0-5 °C) Saturated sodium chloride solution	12 L	1.8 kg Sodium chloride dissolved 10 lit process water lot-1
11.	Take back the organic layer into pre cooled reactor to 0- 5 $^{\circ}\mathrm{C}$		
12.	Charge powdered anhydrous CaCl ₂	1.2 kg	
13.	Stir the reaction mixture at 0-5 °C for 10-15 min		
14.	Submit the sample to QC for the strength (keep the sample at 2-8 °C) & Moisture content		Approximate concentration of monochloramine solution 3-5% (Chlorine content), Moisture content NMT 0.5%
15.	Keep the reaction mixture in the reactor at -5 to 0 °C until to charge into Part-B		
16.	Part-B: Preparation of pyrrolo[2,1-f][1,2,4]triazin-4- amine (RMD-B-II)		
17.	Check the cleanliness of the reactor-2		
18.	Charge DMF (Lot-1) into the reactor under nitrogen atmosphere at 25-30 °C	6.0 L	
19.	Cool the reactor to 0-5 °C		
20.	Charge Sodium hydride (60 % dispersion in mineral oil) into the reactor keeping the internal temperature between 0-5 °C	0.29 kg	
21.	Stir the reaction mixture at 0-5 °C for 20-30 min		
22.	Charge Pyrrole-2-carbonitrile into the reaction mixture maintaining the internal temperature at 5-10 °C under nitrogen atmosphere	0.60 kg	Gas evolution observe
23.	Stir the reaction mixture at 0-5 $^{\circ}$ C for 30-40 min under N ₂ atmosphere		
24.	Charge above prepared Monochloramine solution in MTBE into the reaction mixture while maintaining the internal temperature between 0-5 °C	24.0 L	Reaction mass becomes yellowish to brown colour





25.	Send the sample for HPLC analysis to check the consumption of Pyrrole-2-carbonitrile (IPC-1). Sample preparation: Take the sample directly from reaction mixture and submit		IPC-1: Pyrrole-2- carbonitrile NMT 3.0% Result: IPC-01: Comp-2: 1.31%
26.	After HPLC complies, charge Formamidine acetate at $0-5 \ ^{\circ}\text{C}$	2.04 kg	
27.	Heat the reaction mixture 85-90 °C and simultaneously distil the MTBE at atmospheric pressure until internal temperature reaches to 85-90 °C		
28.	Stir the reaction mixture for 20 h at 85-90 °C		
29.	Send the reaction mixture sample for HPLC analysis to check the consumption of RMD-B-IIa Sample preparation: Take the sample directly from reaction mixture and submit		IPC-2: Comp-3 content NMT 2.0% Result: 0.14%
30.	After complies of the HPLC results, cool the reaction mixture at 25-30 °C		
31.	Filter the reaction mixture		
32.	Wash the bed with DMF (Lot-2)	0.6 L	
33.	Concentrate the filtrate containing DMF up to \sim 4V under reduced pressure at below 70 °C		
34.	Cool the reaction mixture to 25-30 °C		
35.	Charge the water slowly (Lot-2)	2.4 L	
36.	Stir the reaction mixture for 1 h at 25-30 °C		
37.	Cool the reaction mixture and further stir for 2.0 h at 5-10 $^{\circ}\mathrm{C}$		
38.	Stop the stirring, filter the reaction mixture		
39.	Wash the wet solid with water (Lot-3)	0.6 L	
40.	Suck dry the wet solid for 30-45 min		
41.	Slurry wash the wet solid with MTBE (Lot-2)	1.2 L	
42.	Suck dry the wet solid for 1 h		
43.	Unload the wet solid and charge into dryer		
44.	Dry the material for 5-6 h under vacuum at 50-55 °C still constant weight		
45.	Pack the dry material under nitrogen atmosphere in LDPE transparent bag and followed by LDPE black bag and tie with pp strap and keep in HDPE drum.		
46.	Store the material in dark and dry place at ambient temperature		
47.	Yield	0.69 kg	67%





S. No.	Batch Id	IPC-1 (Limit: NMT 3.0 %)	IPC-2 (Limit: NMT 2.0 %)	Purity by HPLC
1	CR592-15374-10	1.51%	Below the detection level	IPC-1 IPC-2
2	CR592-15288-28	1.31%	0.14%	IPC-1

Results of two batches:

S. No	Batch No.	Input (g)	Output (g)	Molar Yield	Analytical data
1	CR592-15374-10	500.0	590.0	68%	CR592-15374-10
2	CR592-15288-28	600.0	690.0	67%	CR592-15288-28

* Both the batches are of grey coloured and assay 96-97.5%

In an effort to improve the colour and assay , both the batches were mixed and once again purified to afford the desired compound in light brown colour with assay 98.4%. Details are shown below.

Purification detail:

Crude Aminotriazine (550 g, B. No. CR595-15374-10 & 650 g B. No CR592-15288-28), and DMF (4.8 L) were heated to 80°C to afford a clear solution. Reaction mass was cooled to 25-30°C and water (18L) was added to get a thick slurry which was aged at same temperature for 1.0 h and cooled to 0-5°C and stirred for 4 h and filtered and washed with 1V (1.2 L) of MTBE and dried the solid under vacuum at 50-55 °C for 6h till constant weight

Y = 1050 g (87.5%)

Analytical data:







Results and discussion

Optimization of Step-1:

1) 2)	POCl ₃ (1.1 eq), DMF, 1 (1 eq), 20 °C, 1 h	<u>∥</u> N
NH 3) 4)	H ₂ O (3 V) NH ₂ OH.HCI (1.2 eq), Base, Additive	NH
1 <i>H-</i> pyrrole Molecular Weight: 67.09	Step-1	1 <i>H-</i> pyrrole-2-carbonitrile Molecular Weight: 92.10
1		2

General protocol: Without any base and additive

POCl3 (1.1 eq) was added to DMF (15V) slowly at 0°C for 30 min, Pyrrole (100 g, 1 eq) stirred for 1 h at 0 °C. RM was warmed to RT and H2O (3V) was added and stirred for 30 min and NH2OH.HCl (1.2 eq) was added and stirred at 70-80 °C.

Comparative data:

Batch No	Input	Output (Yield)	DMF (V)	Data
CR592-15288-5	100 g	126.3 g (92.0%)	15	Crude purity: 96% (by GC)-SMI- 2.7%





CR592-15274-28	25.0 g	32.0 g (93.5%)	10	Crude purity: ~95 % (by GC)-SMI- 3.5%
CR592-15274-29	25.0 g	30.3 g (88.3%)	5	Crude purity: 87 % (by GC)- SMI- 9%

As the reaction performed well, it was further scaled up to 500.0 g scale using 10 V of DMF. Details are shown below.

Batch No	Input	Out put- % yield	Remark/Analytical data
	(Pyrrole)		
CR592-	500.0g	853 g	IPC-01: Pyrrole consumed completely
15288-8		HPLC assay = 50%	IPC-02: after 12 h – Int-Aldehyde
		Assay based yield = 62%	Consumed and could see 93.62%
			Product & SMI 2.57% (Amide impurity)
			pH of RM - 1-2
			HPLC :
			93.70%, SMI 1.57%.
			HPLC crude Assay: 49.4%
			Observation: RM was dark and found difficulty while layer separation. Aq. Layer contains product. Crude was <u>very dark</u> in colour







As the reaction showed difficulty in layer separation and formation of problematic black coloured solid impurities (probably polypyrrole and its derivatives), it was assumed that basic nature may help to prevent the formation of polymeric impurities, reaction was tried in presence of NaOAc and results are shown below.

General protocol: With NaOAc

POCl3 (1.1 eq) was added to DMF (10V) slowly at 0°C for 30 min, Pyrrole (1 eq) stirred for 1 h at 0 °C. RM was warmed to RT and H2O (3V) was added and stirred for 30 min and Sodium acetate (4 eq) and NH2OH.HCl (1.2 eq) was added and stirred at 70-80 °C.

Work up: <u>RM was filtered</u> added water (20V), aqueous layer extracted with EA (20V x 4). EA layer washed with saturated brine solution (20V) and concentrated the EA layer under reduced pressure.

Result:

Batch No	Input	Assay based Yield%	Solvent & Base	HPLC Purity	Remarks
CR592- 15274-68	25.0 g	88	DMF (5 V), & Sodium acetate (4 eq)	94.14%, SMI 3.11%	Scale up from 25.0 g to 500.0 g produces
CR592- 15274-75	500.0 g	92	DMF (5 V) & Sodium acetate (4 eq)	95.12%, SMI 2.25%	consistent yield and purity

Crude colour: Brown, layer separation was comparatively easy



Based on the initial result, reaction was scaled up to 1.0 Kg and details are shown below.

Batch	Input	Out put- % yield	Remark/Analytical data
No	(Pyrrole)		





CR592- 15288- 22	IPC-01: No pyrrole was observed after 1h IPC-02: after 12 h HPLC 93.50%, SMI 2.57% Observation: Excessive black junk material formation was observed and did not observe clear layer separation using DCM. Modified work up protocol: Added chilled (5-10 °C) water (20V), and added MTBE (30V), stirred for 30 min and filtered the RM to remove the solid waste and separated the layers and further aqueous layer extracted with MTBE (10V) and MTBE layer was washed with 10% aqueous sodium bicarbonate solution (30V) and concentration of MTBE layer afforded the crude product Crude Purity by HPLC (area%): 93.66% Assay = 83% DMF assay = 0.1%
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In an effort to further ease the isolation as well as scalable process, the reaction was tried in presence of Pyridine and acetic anhydride and comparative results are shown below.

Batch Ref	Scale	IPC	Chemical purity (A%) by HPLC(after crude work up)	Yield/Assay	Remarks
CR592-15288- 22 (NaOAc batch)	1 Kg	~94% product with SMI-2.5% (SM consumed)	94 %, SMI 2.36%	Assay based yield-83 % 1.288 Kg	More polymeric junk formation was observed
CR592-15288- 25 (Py/Ac2O)	1 Kg	~98% product with SMI-0.8% (SM consumed)	98%, SMI 0.65%	Assay based yield-83 % 1.288 Kg	Ease of work up *

* No filtration of reaction mass which help to reduce the cycle time by minimizing one unit operation and eventually minimizes the handling loss of the product on scale up





Potential impurities and their origin

Name	Structure	Origin
Pyrrole	N H	Process impurity/Un-reacted Starting material
1H-pyrrole-2-carbaldehyde	N N N N N N N N N N N N N N N N N N N	Process impurity/Un-reacted intermediate
1H-pyrrole-2-carboxamide	NH ₂	Process impurity/hydrolyzed product





1H-pyrrole-2-carboxamide has been proposed based on the LCMS data.



Auto-Scaled Chromatogram





Optimization of Step-2:



Screening of bases for the N-amination reaction:

Step- No/Batch No	Input Comp- 2	Protocol	Remark/Analytical data
CR592- 15274-73	25.0 g	To a stirred solution of 2- cyanopyrrole (1.0 eq) in DMF (10 V) was added 60%NaH (1.5 eq) at 0-5 °C and the reaction was stirred for 30 min at 10-15 °C temperature. NH2C1 (50V of MTBE solution, assay 4.6%) was added via syringe at 10-15 °C.	IPC-01: Comp-3 (92.85%), comp-2 (2.6%), SMI (3.37%)
CR592- 15274-64	2.0 g	NaH (2.0eq). Other parameters are same	IPC-01: Comp-3 (85%), comp-2 (5%)
CR592- 15274-7	1.0 g	K ^t BuO (2.0 eq)	IPC-01: Comp-3 (26.5%), comp-2 (65.5%)
CR592- 15274-8	1.0 g	Na ^t OBu (2 eq)	IPC-01: Comp-3 (32%), comp-2 (57%)
CR592- 15274-9	1.0 g	Na ^t OAm (2 eq)	IPC-01: Comp-3 (38.8%), comp-2 (53%)





CR592- 15274-34	1.0 g	KOH (1.5 eq)	IPC-01: Comp-3 (50%), comp-2 (46.6%)
Abo	ove reaction	ns showed that N-amination works	well using NaH (1.5 eq) in DMF

Critical observation regarding excess addition of NH2Cl in the reaction mass:

Following reaction was performed to assess the impact of addition of excess NH2Cl to push for the complete consumption of compound-2



Batch No	Input Comp-2	Protocol	Remark/Analytical data
CR592- 15274- 59	1.0 g	To a stirred solution of 2-cyanopyrrole (1.0eq) in DMF (10 V) was added 60%NaH (1.5 eq) and the reaction was stirred for 30 min at ambient temperature. NH2Cl (17V of MTBE solution, assay ~5.0%) was added via syringe. NH2Cl/MTBE was added lot wise (17V) after distilling MTBE	IPC data showed steady decease of SM up to 3 rd lot addition of NH2Cl. Afterwards degradation of product formed was observed. Needs to be investigated before scale up.

NH2C1-MTBE solution	% of Un-reacted SM	% Product	Major Impurities
After Lot-1 addition	64%	30%	
After Lot-2 addition	17%	74%	
After Lot-3 addition	15%	81%	

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After Lot-4 addition	53%	15%	18% & 5%



To prove the hypothesis that compound-3 reacts with excess NH2Cl in absence of base to generate impurities, compound-3 was isolated by quenching the reaction with aq. Na2S2O3 and reacted with NH2Cl. Observation of the reaction is shown below.





Excess NH2Cl generates back compound-2 along with other impurities.

So after 80-90% conversion of compound-2, excess NH2Cl should be added with extreme care. It needs further optimization.

Trail batches data of final Target compound synthesis

General reaction protocol:

To a stirred solution of 2-cyanopyrrole (1.0eq) in DMF (10 V) was added 60%NaH (1.5 eq) at 0-5 °C and the reaction was stirred for 30 min at 10-15 °C temperature. NH2Cl (50V of MTBE solution, assay 3.5%) was added at 10-15 °C. Stirred 15 min at 10-15 °C, RM was monitored and Comp-2 ~1.51%, comp-3 ~97.4%. Added formamidineacetate (5 eq, Avra- Commercial Vendor) and distilled off MTBE (by warming the RM from 25 to 90°C under atmospheric condition) and continue stirring at the same temperature for 20 h.

Work up: RM cooled to 25-30°C and filtered to remove undissolved formamidine. Then distilled off DMF (~6V) and water (4 V) was added to afford slurry which was cooled to 5-10°C and aged for 3 h and filtered and waashed with water (2V) and MTBE (2V) and dried under vacuum to afford the target compound.

Batch No IPC-01 IPC-02 Yield (%) Purity Remark Input Comp-2 (Area%) CR592-500.0 g Comp-Comp-3: 68 99.95 With Formamidine 15374-10 2:1.5% BDL acetate from Avra Assay: 96% (Assay 95%) Comp-3:97%

Summary of the lab batches data:





CR592- 15274-85	100.0 g	Comp- 2: 1.31%, Comp- 3: 95.80%	Comp-3: 0.13%	50	99.44 Assay 97.8%	With Formamidine acetate from Avra (Assay 78%)
CR592- 15274-83	25.0 g	Comp- 2: 0.57%, Comp- 3: 96.85%	Comp-3: 0.10%	66	99.89 Assay 100%	With formamidine acetate from Aldrich(Assay 99%)

In an effort to further reduce the reagent quantities, NaH (1.1 eq vs 1.5 eq) and Formamidine acetate (3.0 eq vs 5 eq) quantities were reduced and the following batches were performed.

Batch No	Input Comp-2	IPC-01	IPC-02	Yield (%)	Purity (Area %)	Remark
CR592- 15365-8	5.0 g	Comp- 2: 0.42% Comp- 3: 96.5%	Comp-3: BDL Target Comp-92%	5.0 g (69)	99.80%	Based on the result another 600.0 g batch was performed
CR592- 15288-28	600.0 g (100% Assay basis) CR592- 15306- 14-F2 260.0 g /Assay 98% CR592- 15288- 25-F3	Comp- 2: 1.31% Comp- 3: 98.22%	Comp-3 0.14%, Target 89.11%	670.0 g (77%),	HPLC (Area%) Purity: 99.87% Assay = 97.50%,	KF = 0.45% Colour grey



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165.0 g /Assay 95%		
CR592- 15306- 15-F2		
189.0 g /Assay 101%		

Impurity profiling of the aminotriazine:



Step- No/Batch No	Input Comp- 2	Protocol	Remark/Analytical data
CR592- 15274-73	25.0 g	To a stirred solution of 2- cyanopyrrole (1.0eq) in DMF (10 V) was added 60%NaH (1.5 eq) at 0-5 °C and the reaction was stirred for 30 min at 10-15 °C temperature. NH2Cl (50V of MTBE solution, assay 4.6%) was added via syringe at 10-15 °C. After comp-2 below 5%, distilled off the MTBE at 25-30 °C and added formamidineacetate (5 eq) and warmed to 80-85°C and stirred for 20 h. Work up: Cooled the RM to below 30°C and added water (20V), solid precipitation was observed. Stirred 1 h at 20-25 °C.	 IPC-01: Comp-3 (92.85%), comp-2 (2.6%), SMI (3.37%) Added Foramidineacetate IPC-02: after 20 h Target- 78.4%, Comp-3 (0.11%), SMI (8.5%) HPLC purity of Targeted compd: 99.79%, SMI 0.15%, Yield : 25.0 g (70~%) KF: 0.96%





	Filtered the solid. Washed the wet solid with MTBE (1V) and dried under vacuum.	

IPC-2:









	Peak Results				
	Name	RT	Area	% Area	RT Ratio
1	Peak1	3.206	45559	0.10	0.274
2	Peak2	3.383	6809	0.02	0.289
3	Peak3	3.648	497433	1.13	0.312
4	Peak4	4.501	10778	0.02	0.384
5	Peak5	4.660	89101	0.20	0.398
6	Peak6	5.974	3748838	8.50	0.510
7	Peak7	7.332	279220	0.63	0.626
8	Peak8	9.470	87948	0.20	0.809
9	Peak9	11.369	16300	0.04	0.971
10	TARGET	11.708	34565955	78.41	1.000
11	Peak11	12.523	10456	0.02	1.070

	r can negung				
	Name	RT	Area	% Area	RT Ratio
12	Peak12	13.596	17545	0.04	1.161
13	Peak13	13.758	33214	0.08	1.175
14	Peak14	14.528	563696	1.28	1.241
15	Peak15	15.043	16530	0.04	1.285
16	Peak16	15.465	17211	0.04	1.321
17	Peak17	15.695	159591	0.36	1.341
18	COMP-3	16.155	47185	0.11	1.380
19	Peak19	16.575	10516	0.02	1.416
20	Peak20	16.831	161255	0.37	1.438
21	Peak21	17.539	10012	0.02	1.498
22	Peak22	17.670	11499	0.03	1.509
23	Peak23	19.727	3173142	7.20	1.685
24	Peak24	19.973	441158	1.00	1.706
25	Peak25	32.445	61331	0.14	2.771

Two major impurities were observed.

5.97 min RT ~9% which corresponds to DMF

19.727 min RT ~7%

Impurity @ 19.727 min got enriched in the MTBE layer and isolated from the same and characterized by 1H & 13CNMR, LCMS.

It was further synthesized and RT was matched.

Structure of the impurity is shown below



Molecular Weight: 162.20



13C NMR









Protocol:

Comp-3 (1.0 eq, 5.0 g), MgSO4 (5.0eq), AcOH (1.0 eq), DMF-DMA (1.3 eq), DCM (11.0V), N2, 25-30°C, 12 h comp-3 converted to DMF-Impurity (As monitored by HPLC, 92% and ~6% comp-3)

Ref: Organic Letters, 22(3), 1217-1221; 2020





	SAMPLE	INFORMATIC	N
Sample Name:	CR592-15380-01-cr	Acquired By:	AM0113345
Sample Type:	Unknown	Sample Set Name:	TCGLS_050920
Vial:	37	Acg. Method Set:	REM KSM DEV 2
Injection #:	1	Processing Method	REMKSM
Injection Volume:	10.00 ul	Channel Name:	250.0nm
Run Time:	45.0 Minutes	Proc. Chnl. Descr.:	2998 PDA 250.0 nm (2998
Date Acquired: Date Processed:	05-09-2020 18:17:43 IST 08-09-2020 07:03:05 IST	Column Name: SHIM	IPACK SOLAR C18(250*4.6)5µ



Peak Results

	Name	RT	Area	% Area	RT Ratio
1	Peak1	3.692	18401	0.70	0.232
2	Peak2	9.274	6462	0.25	0.583
3	Peak3	13.527	9076	0.35	0.850
4	COMP-3	15.912	163559	6.24	1.000
5	Peak5	17.524	20891	0.80	1.101
6	IMP	19.690	2388408	91.14	1.237
7	Peak7	25.230	7743	0.30	1.586
8	Peak8	27.130	6063	0.23	1.705



In few batches another impurity was observed at 1.3 RRT which could not be isolated but analyzed by LCMS and data is shown below.





This impurity most probably formed due to presence of un-reacted NH2Cl which can act as chlorinating agent.





Safety studies of the finalized scheme: RC-1 studies

Step-1



RC-1 report using Py/Ac2O and 10 of DMF

1.0 Subject/Aim: To evaluate the thermal risk factors i.e. heat of reaction, Adiabatic Temperature and MTSR (Maximum temperature of the synthesis reaction).

2.0 Route of synthesis (ROS)



3.0 Brief Process

1.0 Reaction: Charged DMF (as per B.Size : 50 grams) into the reactor at 25-30°C then Cool the solvent to 0°C. Slowly added POCL3 into the reaction mass at 0°C after addition maintained the reaction mass for 30 min.

Slowly added 1H-pyrrole into the Reaction mass at 0°C after addition maintained the reaction mass for 60 min. Drop wise added water into the reaction mass then maintained the mass for 30 min.





Added Acetic anhydride followed by pyridine at 0°C then maintained the reaction mass for 10 min after that added NH2OH.HCl to the reaction mass at 0°C and maintained for 30 min. Charged in 4 equal lots of Sodium acetate into the reaction at 0°C and maintained the mass for 30 min.

4.0 Raw materials used:

S.No	Raw materials Name	Molecular weight	Quantities	Equiv.
1	1H-pyrrole	67.09	50.0 g	1.0
2	POCI3	153.33	125.70 g	1.1
3	DMF	73.09	500 ml	10V
4	Water	18.00	150 ml	3V
5	NH2OH.HCI	69.49	62.15 g	1.2
6	Pyridine	79.10	295 g	5.0
7	Acetic anhydride	102.09	91.30 g	1.2

5.0 RC1 Study: Process Observations: B.Size 50 grams of 1H-pyrrole

Process	Observations
Charged DMF (500 ml)into the reactor at 25°C	Homogeneous clear solvent
Cool the reaction mass to 0°C	Homogeneous clear solvent
Calibrate it to find out UA & Cp values	Establish the base line and predict specific heat.
Slowly added POCl3 (125.70 g) into the reactor at 0°C over 15 min.	Homogeneous mass with light yellow color Observed high temperature raise during addition, Controlled addition is to be done. Gas liberation observed during addition
Maintain the reaction mass at 0°C over 30 min.	Homogeneous mass with light yellow color Reagent thermal accumulation at the end of dosing is 1.80%.
Drop wise added 1H-pyrrol (50 g) into the reactor at 0°C.	Homogeneous mass with dark orange color. Over all addition should be controlled even single drop addition shows high rise in reaction temperature.
Maintain the reaction mass at 0°C over 60 min.	Homogeneous mass with dark orange color. Reagent thermal accumulation at the end of dosing is 0.80%.





Drop wise added water (150 ml) into the reactor at 0°C.	Homogeneous mass with dark orange color. Over all addition should be controlled even single drop addition shows high rise in reaction temperature.
Maintain the reaction mass at 0°C over 60 min.	Homogeneous mass with dark orange color. Reagent thermal accumulation at the end of dosing is 1.86%.
Drop wise added pyridine (295 g) over 32 min into the reactor at 0°C and maintained for 10 min.	Homogeneous mass with dark orange color. Reagent thermal accumulation at the end of dosing is 0%.
Drop wise added Acetic Anhydride (91.30 g) over 10 min into the reactor at 0°C and maintained for 10 min.	Homogeneous mass with dark orange color. Reagent thermal accumulation at the end of dosing is 1.80%.
Slowly added NH2OH.HCl (62.15 g) into the reactor at 0°C.	Heterogeneous mass with dark orange color Initially heat of reaction is endothermic after addition shows exothermic reaction Addition should be in lot wise addition
Maintain the reaction mass at 0°C over 10 min.	Heterogeneous mass with dark orange color Reagent thermal accumulation at the end of dosing is 96.50%.
Calibrate it to find out UA & Cp values	Establish the base line and predict specific heat.
Heat the reaction mass to 90°C.	Heterogeneous mass with dark yellow color
Maintain the reaction mass at 90°C over 12 hr.	During heating maintenance dark yellow color turns to blackish color with heterogeneous mass nature There is no abnormal heat liberation was observed Heating maintenance was in smooth run and stable temperature.
Cool the reaction mass to 30°C.	Remains blackish color with heterogeneous mass nature
Unloaded the reaction mass	Remains blackish color with heterogeneous mass nature









Rc1e Technical Data: During addition of POCL3 at 0°C.





RC parameters Results		Remarks/Recommendations
Heat generated	49.08 KJ/ 50 grams of KSM 65.88 KJ/mole of KSM	Heat of reaction shows is mild exothermic considerable adiabatic temp rise is 30.40 °C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	30.40	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done
MTSR (°C) (As per 100% accumulation)	30.40°C (0 +30.40)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of reaction is less than MTT, so reaction safe for scale-up point of view
Thermal Accumulation at the end of Dosing	1.80 %	End of the dosing thermal accumulation is Considerable low
Thermal Conversion at the end of Dosing	98.20%	End of the dosing thermal Conversion is high
Specific Heat Before Reaction (kJ/Kg K) 2.83		Specific heat of reaction is high and it can
Specific Heat After Reaction (kJ/Kg K)	1.95	slowly achieving temp due to high energy requirement.





RC1 Graph: 1H-pyrrole addition shows Exotherm



Rc1e Technical Data: During addition of <u>1H-pyrrole</u> at 0°C.





RC parameters	Results	Remarks/Recommendations
Heat generated	144.73 KJ/ 50 grams of KSM 194.27 KJ/mole of KSM	Heat of reaction shows is exothermic considerable adiabatic temp rise is 84.54 °C. The addition should be controlled due exothermic reaction.
Adiabatic temp rise (K)	84.54	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done
MTSR (°C)	84.54°C (0 + 84.54)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of the reaction is greater than MTT
Thermal Accumulation at the end of Dosing	0.80 %	End of the dosing thermal accumulation is Considerable low
Thermal Conversion at the end of Dosing	99.20 %	End of the dosing thermal Conversion is high
Specific Heat Before Reaction (kJ/Kg K)	2.83	Specific heat of reaction is high and it can
Specific Heat After Reaction (kJ/Kg K)	1.95	accomplish medium heat transfer rate and achieving temp due to high energy requirement.





RC1 Graph: Water addition shows Exotherm



Rc1e Technical Data: During addition of water at 0°C.

RC parameters	Results	Remarks/Recommendations	
Heat generated	91.90 KJ/ 50 grams of KSM 123.35 KJ/mole of KSM	Heat of reaction shows is mild exothermic considerable adiabatic temp rise is 46.63°C. The addition should be controlled due to exothermic reaction.	
Adiabatic temp rise (K)	46.63	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done	
MTSR (°C)	46.63°C (0 +46.63)	Addition should be under double valve control.	
MTT (°C)	152°C	The MTSR of the reaction is less than MTT	
Thermal Accumulation at the end of Dosing	1.86 %	End of the dosing thermal accumulation is Considerable low	
Thermal Conversion at the end of Dosing	98.14 %	End of the dosing thermal Conversion is high	
Specific Heat Before reaction (kJ/Kg K) 2.83		Specific heat of reaction is high and it can	
Specific Heat After reaction(kJ/Kg K)	1.95	accomplish medium heat transfer rate and slow achieving temp due to high energy requirement.	



RC1	Grap	bh:	Acetic	Anhy	/dride	addition	shows	Exotherm

RC parameters	Results	Remarks/Recommendations
Heat generated	160.52 KJ/ 50 grams of KSM 215.46 KJ/mole of KSM	Heat of reaction shows is exothermic considerable adiabatic temp rise is 68.85°C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	68.85	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done
MTSR (°C)	68.85°C (0 +68.85)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of the reaction is greater than MTT
Thermal Accumulation at the end of Dosing	0 %	End of the dosing thermal accumulation is Considerable low
Thermal Conversion at the end of Dosing	100 %	End of the dosing thermal Conversion is high
Specific Heat Before reaction (kJ/Kg K)	2.83	Specific heat of reaction is high and it can
Specific Heat After reaction(kJ/Kg K)	1.95	accomplish medium heat transfer rate and achieving temp due to high energy requirement.



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Rc1e Technical Data: During addition of <u>Acetic Anhydride</u> at 0°C.

RC1 Graph: NH2OH.HCl addition shows Exotherm

RC parameters	Results	Remarks/Recommendations
Heat generated	23.75 KJ/ 50 grams of KSM 31.88 KJ/mole of KSM	Heat of reaction shows is mild exothermic nature considerable adiabatic temp rise is 9.88°C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	9.88	Adiabatic temp rise shows low hazard in reaction, controlled addition to be done
MTSR (°C)	9.88°C (0+9.88)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of the reaction is less than MTT
Thermal Accumulation at the end of Dosing	1.85 %	End of the dosing thermal accumulation is Considerable medium To be add sodium acetate for longer hours
Thermal Conversion at the end of Dosing	98.15 %	End of the dosing thermal Conversion is medium
Specific Heat Before reaction (kJ/Kg K)	2.83	Specific heat of reaction is high and it can
Specific Heat After reaction(kJ/Kg K)	1.95	accomplish medium heat transfer rate and slow achieving temp due to high energy requirement.



Rc1e Technical Data: During addition of NH2OH.HCl at 0°C.

RC1 Graph: graph for reaction maintenance for 14 hrs

RC parameters	Results	Remarks/Recommendations
Heat generated	23.32 KJ/ 50 grams of KSM 31.30 KJ/mole of KSM	Initially heat of reaction is endothermic after addition shows exothermic reaction
Adiabatic temp rise (K)	9.96	Adiabatic temp rise shows low hazard in reaction, controlled addition to be done
MTSR (°C)	9.96°C (0+9.96)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of the reaction is less than MTT
Thermal Accumulation at the end of Dosing	96.50 %	End of the dosing accumulation of reagent is high , so add reagent in equal lot wise
Thermal Conversion at the end of Dosing	3.50 %	End of the dosing thermal Conversion is medium
Specific Heat Before reaction (kJ/Kg K)	2.83	Specific heat of reaction is high and it can
Specific Heat After reaction(kJ/Kg K)	1.95	accomplish medium heat transfer rate and slow achieving temp due to high energy requirement.



Observation : There is no abnormal heat liberation and internal temperature raise observed

6.0 Conclusion and Recommendation:

- Addition of POCI3 at 0°C shows mild exothermic and indicates Low severity reaction with adiabatic temperature rise of 30.40°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 30.40°C.
- 2. Recommended for POCI3 charging should be through double controlled valve under nitrogen atmosphere.
- 3. Recommended for during addition of POCI3 into The reactor condenser vent should be connected to the Scrubber.
- 4. Ensure Condenser efficient cooling before startup the addition of POCL3.
- 5. Addition of 1H-pyrrol at 0°C shows Exothermic and indicates Medium severity reaction with adiabatic temperature rise of 84.54°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 84.54°C.
- 6. Recommended for 1H-pyrrol charging should be through double controlled valve under nitrogen atmosphere.
- 7. Ensure Condenser efficient cooling before startup the addition of 1H-pyrrol.
- 8. Addition of Water at 0°C shows Exothermic and indicates Medium severity reaction with adiabatic temperature rise of 46.63°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 46.63°C.
- 9. Recommended for Water charging should be through double controlled valve.
- 10. Ensure Condenser efficient cooling before startup the addition of water.
- 11. Addition of Pyridine at 0°C shows Exothermic and indicates Medium severity reaction with adiabatic temperature rise of 68.85°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 68.85°C.
- 12. Addition of Acetic anhydride at 0°C shows mild Exothermic and indicates low severity reaction with adiabatic temperature rise of 9.88°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 9.88°





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- 13. Addition of NH2OH.HCl at 0°C shows mild Exothermic and indicates low severity reaction with adiabatic temperature rise of 9.96°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 9.96°C.
- 14. Recommended for NH2OH.HCI_charging should be through double valve Hopper and in equal lot wise addition to avoid thermal accumulation of reagent as per RC shows 96.50% thermal accumulation at the end of dosing.

7.0 Reference

1. Thermal safety of Chemical Processes (Risk assessment and Process Design By Francis Stoessels

<u>RC-1</u> study of Step-1 using 5V DMF and NaOAc base

4.0 Subject/Aim: To evaluate the thermal risk factors i.e. heat of reaction, Adiabatic Temperature and MTSR (Maximum temperature of the synthesis reaction).

5.0 Route of synthesis (ROS)



6.0 Brief Process

2.0 Reaction: Charged DMF (as per B.Size : 100 grams) into the reactor at 25-30°C then Cool the solvent to 0°C. Slowly added POCL3 into the reaction mass at 0°C after addition maintained the reaction mass for 30 min. slowly added 1H-pyrrole into the Reaction mass at 0°C after addition maintained the reaction mass at for 60 min. Drop wise added water into the reaction mass then maintained the mass at for 60 min. after that added in equal lots of NH2OH.HCl to the reaction mass at 0°C and maintained the mass for 30 min. Charged in 4 equal lots of Sodium acetate into the reaction at 0°C and maintained the mass for 30 min.

4.0 Raw materials used:

S.No	Raw materials Name	Molecular weight	Quantities	Equiv.
1	1H-pyrrole	67.09	100.0 g	1.0



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2	POCI3	153.33	251.36 g	1.1
3	DMF	73.09	500 ml	5V
4	Water	18.00	300 ml	3V
5	NH2OH.HCI	69.49	124.28 g	1.2
6	CH3COONa	77.08	459.56 g	4.0

5.0 RC1 Study: Process Observations: B.Size 100 grams of 1H-pyrrole

Process	Observations
Charged DMF (500 ml)into the reactor at 25°C	Homogeneous clear solvent
Cool the reaction mass to 0°C	Homogeneous clear solvent
Calibrate it to find out UA & Cp values	Establish the base line and predict specific heat.
Slowly added POCl3 (251.36 g) into the reactor at 0°C.	Homogeneous mass with light yellow color Observed high temperature raise during addition, Controlled addition is to be done. Gas liberation observed during addition
Maintain the reaction mass at 0°C over 30 min.	Homogeneous mass with light yellow color Reagent thermal accumulation at the end of dosing is 0.53%.
Drop wise added 1H-pyrrol (100 g) into the reactor at 0°C.	Homogeneous mass with dark orange color. Over all addition should be controlled even single drop addition shows high rise in reaction temperature.
Maintain the reaction mass at 0°C over 60 min.	Homogeneous mass with dark orange color. Reagent thermal accumulation at the end of dosing is 0.2%.
Calibrate it to find out UA & Cp values	Establish the base line and predict specific heat.
Raise the reaction mass to 30°C	No impact on raising temperature of the reaction mass
Drop wise added water (300 ml) into the reactor at 30°C.	Homogeneous mass with dark orange color. Over all addition should be controlled even single drop addition shows high rise in reaction temperature.
Maintain the reaction mass at 30°C over 60 min.	Homogeneous mass with dark orange color. Reagent thermal accumulation at the end of dosing is 1.10%.



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Slowly added NH2OH.HCl (124.28 g) in 2 lots equal quantity into the reactor at 30°C.	Heterogeneous mass with dark orange color Addition shows the reaction is endothermic Nature. Addition should be longer hours to reduce thermal accumulation
Maintain the reaction mass at 30°C over 10 min.	Heterogeneous mass with dark orange color Reagent thermal accumulation at the end of dosing is 42%.
Slowly added CH3COONa (459.56 g) in 4 lots equal quantity into the reactor at 30°C.	Heterogeneous mass with dark yellow color Addition should be longer hours to reduce thermal accumulation
Maintain the reaction mass at 30°C over 30 min.	Heterogeneous mass with dark yellow color Reagent thermal accumulation at the end of dosing is 45%.
Calibrate it to find out UA & Cp values	Establish the base line and predict specific heat.
Heat the reaction mass to 90°C.	Heterogeneous mass with dark yellow color
Maintain the reaction mass at 90°C over 12 hr.	During heating maintenance dark yellow color turns to blackish color with heterogeneous mass nature There is no abnormal heat liberation was observed Heating maintenance was in smooth run and stable temperature.
Cool the reaction mass to 30°C.	Remains blackish color with heterogeneous mass nature
Unloaded the reaction mass	Remains blackish color with heterogeneous mass nature

RC1 Graph: Overall Reaction

Trend	Color	Axis	Units
Tr		2	°C
Tj		2	°C
qr_hf		1	W
Vr		3	ml
Tr-Tj		4	К





Rc1e Technical Data: During addition of POCL3 at 0°C.

RC parameters	Results	Remarks/Recommendations
Heat generated	103.60 KJ/ 100 grams of KSM 69.53 KJ/mole of KSM	Heat of reaction shows is exothermic considerable adiabatic temp rise is 68.70 °C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	68.70	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done
MTSR (°C)	68.70°C (0 + 68.70)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of reaction is less than MTT, so reaction safe for scale-up point of view
Thermal Accumulation at the end of Dosing	0.53 %	End of the dosing thermal accumulation is Considerable low
Thermal Conversion at the end of Dosing	99.47%	End of the dosing thermal Conversion is high
Specific Heat Before Reaction (kJ/Kg K)	2.75	Specific heat of reaction is high and it can
Specific Heat After Reaction (kJ/Kg K)	1.81	slowly achieving temp due to high energy requirement.



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RC1 Graph: 1H-pyrrole addition shows Exotherm



Rc1e Technical Data: During addition of <u>**1H-pyrrole**</u> at 0°C.

RC parameters	Results	Remarks/Recommendations
Heat generated	224.82 KJ/ 100 grams of KSM 150.88 KJ/mole of KSM	Heat of reaction shows is exothermic considerable adiabatic temp rise is 150.40°C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	150.40	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done
MTSR (°C)	150.40°C (0 + 150.40)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of the reaction is greater than MTT
Thermal Accumulation at the end of Dosing	0.2 %	End of the dosing thermal accumulation is Considerable low
Thermal Conversion at the end of Dosing	99.80 %	End of the dosing thermal Conversion is high
Specific Heat Before Reaction (kJ/Kg K)	2.75	Specific heat of reaction is high and it can
Specific Heat After Reaction (kJ/Kg K)	1.81	accomplish medium heat transfer rate and achieving temp due to high energy requirement.







Rc1e Technical Data: During addition of water at 30°C.

RC parameters	Results	Remarks/Recommendations
Heat generated	344.62 KJ/ 100 grams of KSM 231.28 KJ/mole of KSM	Heat of reaction shows is exothermic considerable adiabatic temp rise is 187.66 °C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	157.66	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done
MTSR (°C)	187.66°C (30 + 157.66)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of the reaction is less than MTT
Thermal Accumulation at the end of Dosing	1.10 %	End of the dosing thermal accumulation is Considerable low
Thermal Conversion at the end of Dosing	98.90 %	End of the dosing thermal Conversion is high
Specific Heat Before reaction (kJ/Kg K)	1.81	Specific heat of reaction is high and it can
Specific Heat After reaction(kJ/Kg K)	2.20	accomplish medium heat transfer rate and slow achieving temp due to high energy requirement.

RC1 Graph: NH2OH.HCl addition shows Exotherm



Rc1e Technical Data: During addition of <u>NH2OH.HCl</u> at 30°C.

RC parameters	Results	Remarks/Recommendations
Heat generated	19.84 KJ/ 100 grams of KSM 13.31 KJ/mole of KSM	Heat of reaction shows is endothermic nature considerable adiabatic temp rise is -7.95°C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	-7.95	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done
MTSR (°C)	22.05°C (30 – 7.95)	Maintain temperature during addition due to endothermic reaction
MTT (°C)	152°C	The MTSR of the reaction is less than MTT
Thermal Accumulation at the end of Dosing	42.22 %	End of the dosing thermal accumulation is Considerable low
Thermal Conversion at the end of Dosing	57.78 %	End of the dosing thermal Conversion is high
Specific Heat Before reaction (kJ/Kg K)	1.81	Specific heat of reaction is high and it can
Specific Heat After reaction(kJ/Kg K)	2.20	accomplish medium heat transfer rate and slow achieving temp due to high energy requirement.



Rc1e Technical Data: During addition of <u>NaOAc</u> at 30°C.

RC1 Graph: graph for reaction maintenance for 12	hrs
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RC parameters	Results	Remarks/Recommendations
Heat generated	26.67 KJ/ 100 grams of KSM 17.90 KJ/mole of KSM	Heat of reaction shows is mild exothermic nature considerable adiabatic temp rise is 7.08°C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	7.08	Adiabatic temp rise shows low hazard in reaction, controlled addition to be done
MTSR (°C)	37.08°C (30 + 7.08)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of the reaction is less than MTT
Thermal Accumulation at the end of Dosing	45 %	End of the dosing thermal accumulation is Considerable medium To be add sodium acetate for longer hours
Thermal Conversion at the end of Dosing	55 %	End of the dosing thermal Conversion is medium
Specific Heat Before reaction (kJ/Kg K)	1.81	Specific heat of reaction is high and it can
Specific Heat After reaction(kJ/Kg K)	2.20	accomplish medium heat transfer rate and slow achieving temp due to high energy requirement.



DSC Report : Identify the Probability of Severity





DSC CONCLUSION:

- **1.** As per the DSC Report of the reaction mass after addition of 1H-Pyrrole observed heat liberation observed due to scientifically reason the heat of liberation is for formation of aldehyde and there is no thermal decomposition.
- 2. DSC Report 02 : Reaction mass after Water addition





DSC CONCLUSION:

1. As per the DSC Report of the reaction mass after addition of water observed heat liberation observed due to scientifically reason the heat of liberation is for Pocl3 and water incompatibility under heating, And there is no thermal decomposition in the reaction mass.

Observation : There is no abnormal heat liberation was observed

6.0 Conclusion and Recommendation:

- 1. Addition of POCI3 at 0°C shows exothermic and indicates Medium severity reaction with adiabatic temperature rise of 68.70°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 68.70°C.
- 2. Recommended for POCI3 charging should be through double controlled valve under nitrogen atmosphere.
- 3. Recommended for during addition of POCI3 into The reactor condenser vent should be connected to the Scrubber.
- 4. Ensure Condenser efficient cooling before startup the addition of POCL3.
- 5. Addition of 1H-pyrrol at 0°C shows Exothermic and indicates Medium severity reaction with adiabatic temperature rise of 150.40°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 150.40°C.
- 6. Recommended for 1H-pyrrol charging should be through double controlled valve under nitrogen atmosphere.
- 7. Ensure Condenser efficient cooling before startup the addition of 1H-pyrrol.
- 8. Addition of Water at 30°C shows Exothermic and indicates Medium severity reaction with adiabatic temperature rise of 157.76°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 187.76°C.
- 9. Recommended for Water charging should be through double controlled valve.
- 10. Ensure Condenser efficient cooling before startup the addition of water.





Process safety Evaluation Lab/Kilo Lab



- 11. Addition of NH2OH.HCl_at 30°C shows endothermic and indicates low severity reaction with adiabatic temperature rise of -7.95°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 22.05°C.
- 12. Recommended for NH2OH.HCl_charging should be through double valve Hopper and longer hours addition to avoid thermal accumulation of reagent as per RC shows 42% thermal accumulation at the end of dosing.
- 13. Addition of NaOAc at 30°C shows mild Exothermic and indicates low severity reaction with adiabatic temperature rise of 7.08°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 37.08°C.
- 14. Recommended for NH2OH.HCI_charging should be through double double valve Hopper and longer hours addition to avoid thermal accumulation of reagent as per RC shows 45% thermal accumulation at the end of dosing.

7.0 Reference

1. Thermal safety of Chemical Processes (Risk assessment and Process Design By Francis Stoessels

Software reference document:







1.0 Subject/Aim: To evaluate the thermal risk factors i.e. heat of reaction, Adiabatic Temperature and MTSR (Maximum temperature of the synthesis reaction).

2.0 Route of synthesis (ROS)



3.0 Brief Process

Reaction: Charged NaH and DMF into the reactor at 25°C after that cool the mass to 0°C. Slowly added Pyrrole-2-carbonitrile into the reactor at 0°C after addition maintained the reaction mass for 30 min. Charged NH2Cl in MTBE solution into the reaction mass at 0°C, after addition maintained the reaction mass for 30 min. Reaction was monitored by TLC then charged Formamidine acetate into the mass at 0°C.

4.0 Raw materials used:

Raw materials	Quantity	Molecular weight	Equivalent
Pyrrole-2-carbonitrile	35.0 gm	92.04	1.0eq
60% NaH	22.81 gm	23.99	1.5eq
NH2Cl in MTBE	1.4 Lit	-	40Vol
DMF	350 mL	73.09	10Vol
Formamidine acetate	158 g	104.11	4.0eq

5.0 RC1 Study: Process Observations:

Reaction: B.Size: 35 grams of Pyrrole-2-carbonitrile (STG-02)





Process	Observations
Charged NaH and DMF into the reactor at 25°C	Heterogeneous mass with light ash color
Cool the reaction mass to 0°C	Heterogeneous mass with light ash color
Calibrate it to find out UA & Cp values	Establish the base line and predict specific heat.
Slowly added Pyrrole-2-carbonitrile into the reactor at 0°C.	Heterogeneous mass with Dark ask color Addition Shows exothermic during addition and temperature Max rise up to 55.00 °C. Reagent sudden dump (under Cooling failure) the maximum attainable temperature is 55.00°C
Maintain the reaction mass at 0°C over 30 min.	End of the dosing thermal accumulation is 0% Due to end of addition shows immediate endothermic nature
Charged 1400 ml of NH2Cl in MTBE Solution at 0°C.	Addition Shows low exothermic during addition and temperature Max rise up to 26.40 °C. Reagent sudden dump (under Cooling failure) the maximum attainable temperature is 26.40°C During addition reaction mass changes Heterogeneous Dark ash color to light pink color then changed to off white color. No Gas liberation observed during addition.
Maintain the reaction mass for 30 min at 0°C	Heterogeneous mass with off white Color End of the dosing thermal accumulation is 27.6%
Charged Formamidine acetate into the reactor at 0°C	Addition Shows initially endothermic reaction after end of dosing shows exothermic addition and temperature Max rise up to 1.67 °C. Reagent sudden dump (under Cooling failure) the maximum attainable temperature is 1.67°C
Maintain the reaction mass for 30 min at 0°C	Heterogeneous mass with off white Color End of the dosing thermal accumulation is 19.40%
Calibrate it to find out UA & Cp values	Establish the base line and predict specific heat.
Raised the reaction mass to 30°C.	Remains Heterogeneous mass with off white Color
Unloaded the reaction mass	Remains Heterogeneous mass with off white Color





RCI Graph I: Overall Reaction

Trend	Color	Axis	Units
Tr		2	°C
Tj		2	°C
qr_hf		1	W
Vr		3	ml
Tr-Tj		4	К









Rc1e Technical Data: During addition of <u>Pyrrole-2-carbonitrile</u> at 0°C.

RC parameters	Results	Remarks/Recommendations
Heat generated	33.27 KJ/ 35 grams of KSM 87.55 KJ/mole of KSM	Heat of reaction shows exothermic considerable adiabatic temp rise is 55.00 °C. The addition should be controlled due to exothermic reaction.
Adiabatic temp rise (K)	55.00	Adiabatic temp rise shows medium hazard in reaction, controlled addition to be done
MTSR (°C) (As per 100% Accumulation)	55.00°C (0 +55.00)	Addition should be under double valve control.
MTT (°C)	152°C	The MTSR of reaction is less than MTT, so reaction safe for scale-up point of view
Thermal Accumulation at the end of Dosing	0 %	End of the dosing thermal accumulation is Considerable low After addition shows immediate endothermic nature
Thermal Conversion at the end of Dosing	100 %	End of the dosing thermal Conversion is high
Specific Heat Before Reaction (kJ/Kg K)	1.55	



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Specific Heat After Reaction (kJ/Kg K) 1.52

Specific heat of reaction is low and it can accomplish high heat transfer rate and fast achieving temp due to low energy requirement.

RC1 Graph 1.2: NH2Cl in MTBE Solution shows Exothermic



Rc1e Technical Data: During addition of <u>NH2Cl in MTBE Solution</u> at 0°C.







Rc1e Technical Data: During addition of Formamidine acetate at 0°C.

RC parameters	Results	Remarks/Recommendations	
Heat generated	369947 KU//3355græmssoffKSSWI 11034.0655 KU//modkeodfKSSWI	Heat of reaction shows mild exothermic Heat of reaction shows mild exothermic considerable adiabatic temp rise is 26.40 °C. considerable adiabatic temp rise is 1.67 °C. The addition should be controlled due to The addition should be in lot wise. exothermic reaction.	
Adiabatic temp rise (K)	2166970	Adiabatic temp rise shows low hazard in reaction, controlled addition to be done	
MTSR (°C) (As per 100% Accumulation)	2 6407°C ((0) + 26670))	Slightly temperature raise due to sudden Addition should be under double valve control. charge of reagent	
MTT (°C)	152°C	The MTSR of reaction is less than MTT, so reaction safe for scale-up point of view	
Thermal Accumulation at the end of Dosing	29.65 %	End of the dosing thermal accumulation is Considerable medium	
Thermal Conversion at the end of Dosing	80.53 %	End of the dosing thermal Conversion is medium	
Specific Heat Before Reaction (kJ/Kg K)	1.55	Specific heat of reaction is low and it can	
Specific Heat After Reaction (kJ/Kg K)	1.52	achieving temp due to low energy requirement.	





6.0 Conclusion and Recommendation:

- 1. Addition of Pyrrole-2-carbonitrile at 0°C is medium severity reaction with adiabatic temperature rise of 55.00°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 55.00°C.
- 2. Recommended for Pyrrole-2-carbonitrile charging should be through double controlled valve under nitrogen atmosphere.
- 3. Addition of NH2Cl in MTBE at 0°C is Low severity reaction with adiabatic temperature rise of 26.40°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 26.40°C.
- 4. Observed there is no noticeable gas liberation during addition of NH2Cl in MTBE Solution.
- 5. Addition of Formamidine acetate at 0°C is Low severity reaction with adiabatic temperature rise of 1.67°C. In case of cooling failure or dumping, the maximum temperature attainable by the synthesis reaction mixture is 1.67°C.
- 6. During addition observed initially endothermic reaction then completion slightly exothermic reaction with accumulation of 19.43% so recommended for lot wise addition.
- 7. The reaction is scalable for bigger batch size with RC recommendations.

7.0 Reference

1. Thermal safety of Chemical Processes (Risk assessment and Process Design By Francis Stoessels

Reference Document:



RC software Report:





Further areas of developments / improvements

- ✓ Although the process has been scaled up to kg scale, there is still scope for further improvements
- ✓ Step-1 isolation needs to be further optimized in terms of waste generation, reduction of PMI
- ✓ Step-2 is still run under high dilution which is major road block for further scale up

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Look forward to continue our collaboration further and strengthen our relationship